

KINGDOM OF SAUDI ARABIA
Ministry of Education
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College of Science
Department of Physics



المملكة العربية السعودية
وزارة التعليم
جامعة الإمام محمد بن سعود الإسلامية
كلية العلوم
قسم الفيزياء

Chapter 4

Applications of the second Law of Thermodynamics

المفهوم الرياضي للأنشود.

THE MATHEMATICAL CONCEPT OF ENTROPY

دلالة على الفوضى
[::]
-42

The Clausius's definition of the entropy S is given by:

$$dS = \frac{dQ_r}{T}$$

Where dQ_r is the heat flow into the system for reversible process, and T is the absolute temperature.

When we substitute the precedent equation and the first law of thermodynamic, we obtain, for reversible process:

$$dU = T dS - P dV$$

$$du = dq - w$$

$$du = dST - pdv$$

العمليات عند العكس

IRREVERSIBLE PROCESSES

Consider the following processes and the results observed in nature:

عندما يمر تيار في مقاومة فان الطاقة تتعب من المقاومة و يعود الى قضيعة البطارية

1- A battery will discharge through a resistor, releasing energy.

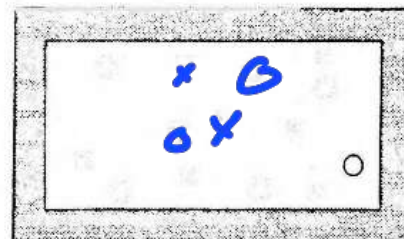
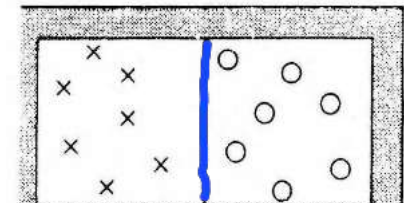
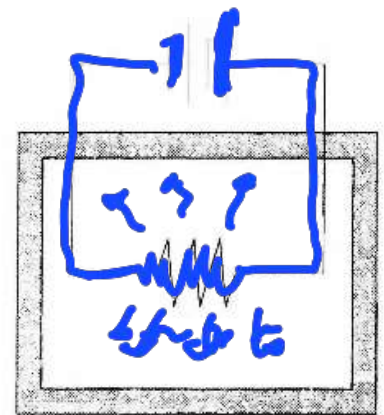
The reverse will not happen adding energy to the resistor by heating will

not cause the battery to charge itself.

خلط الغازات عليه غير عكس

2- Two gases, initially in separate adjoining chambers, will mix uniformly

لا يمكن كحد هذه العملية
(Irreversible)



القانون الثاني لـ Clausius

$$dS = \frac{dQ_r}{T}$$

$$dQ_r = dS T$$

dQ_r : التدفق الحراري في العملية العكسية
 T : درجة الحرارة المطلقة

عند التعويض في القانون الأول حصلنا على:

$$dU = dQ - W$$

$$dU = T dS - P dV \quad \checkmark$$

- لنفرض القانون الثاني في الديناميكا الحرارية
 * أي تغيير تلقائي يجب أن ترافقه زيادة في الانتروبيا

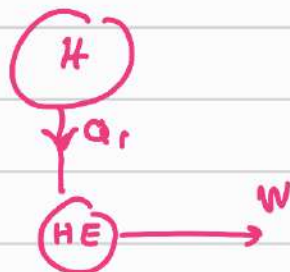
- لنفرض كلاسيكياً

من المستحيل استحداث أي عملية دائرية لنقل الحرارة
 من جسم بارد إلى جسم ساخن بدون عمل تلقائي

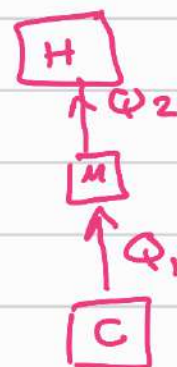
- لنفرض كلفن

من المستحيل تشغيل جهاز حراري يعمل
 على التبادل الحراري مع صندوق حراري واحد

Kelvin



Clausius



مستحيل

IRREVERSIBLE PROCESSES

لن يضغط الغاز نفسه عند مجرد
إزالة الوضع الاصطناعي Irreversible

- 3- A gas in one portion of a chamber is allowed to undergo a free expansion into an evacuated section of the chamber.

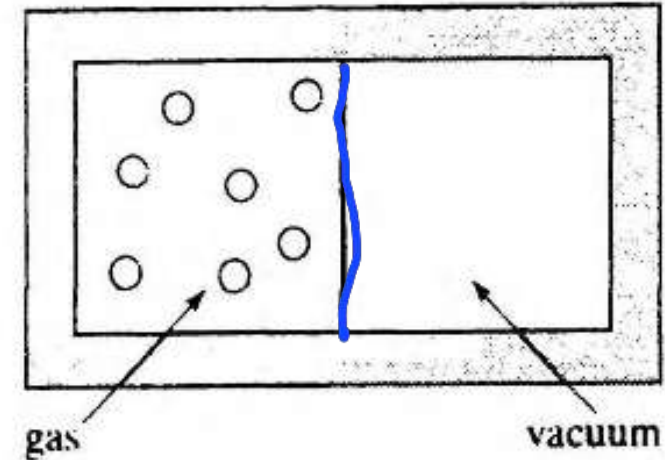
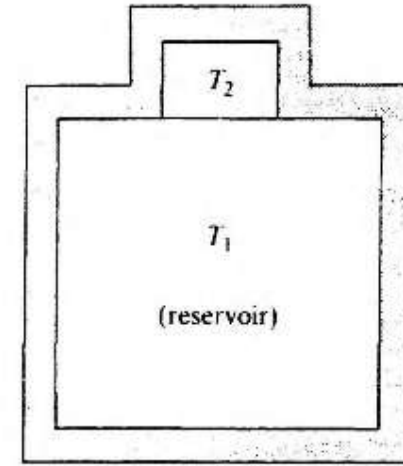
The gas will not compress itself back into its original volume.

- 4- Heat flows from a high temperature body to a low temperature reservoir in the absence of other effects.

The reverse process does not take place.

If $T_2 > T_1$ initially, the body comes to temperature T_1

لا تنتقل الحرارة تلقائياً
من الجسم البارد إلى الساخن

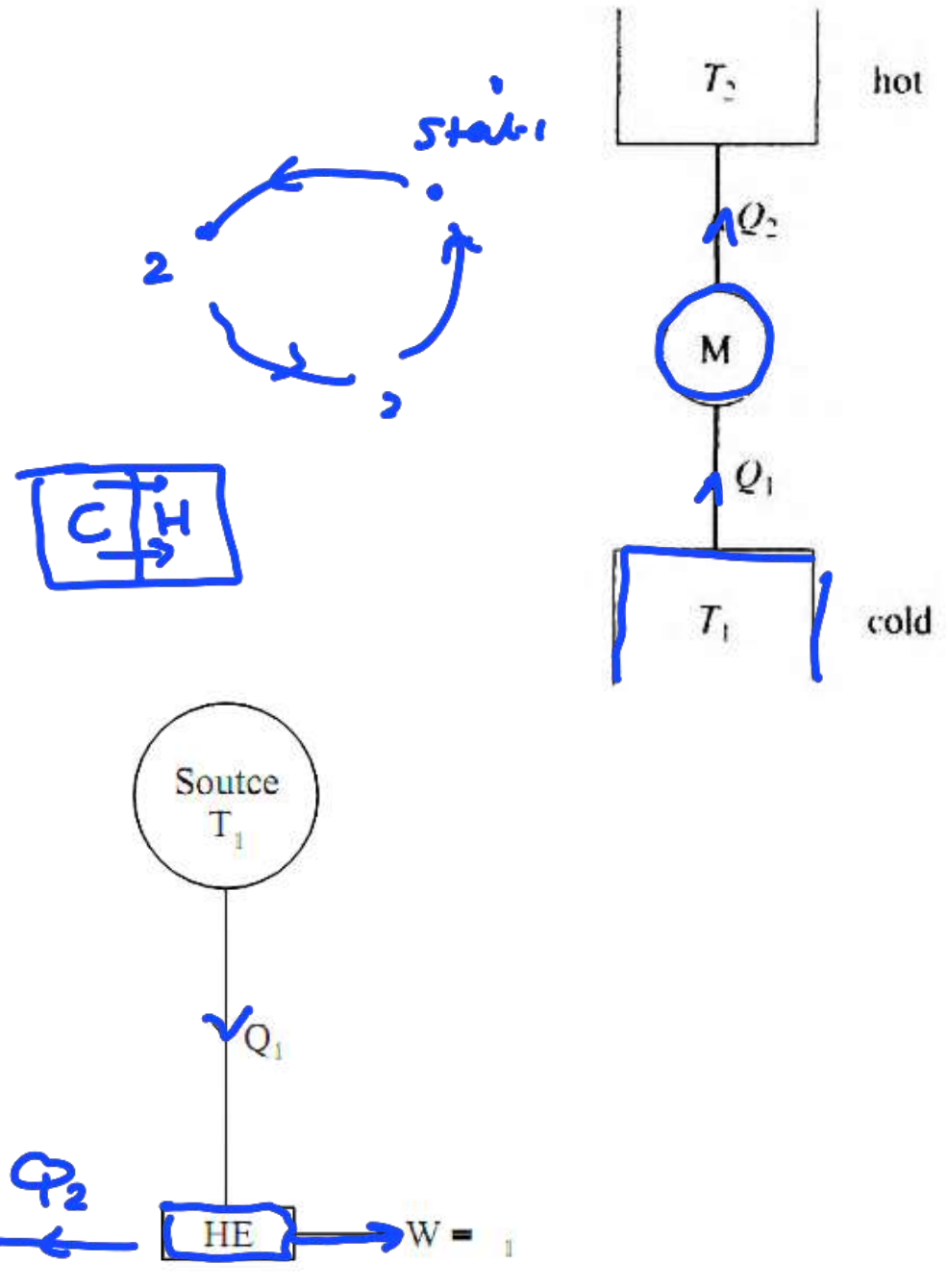


IRREVERSIBLE PROCESSES

In process such as these, the impossibility of the occurrence of the reverse process was first encountered in two famous statements:

Clausius Statement: its impossible to construct a device that operates in cycle and whose sole effect is to transfer heat from a cooler body to hotter body.

Kelvin - Plank Statement: It is impossible to construct a device that operates in a cycle and produces no other effect than the performance of work and exchange of heat with a single reservoir



CARNOT'S THEOREM

احتر محرك كفاءة بين خزانين حراريين هو محرك Carnot

No engine operating between two reservoirs can be more efficient than a Carnot engine operating between those same two reservoirs.

THE CLAUSIUS INEQUALITY AND THE SECOND LAW

For a Carnot cycle we have seen that:

$$\frac{Q_1}{T_1} + \frac{Q_2}{T_2} = 0$$

$\frac{Q}{T}$ معامل Carnot



The quantity Q/T is known as the Carnot ratio. From this we deduced the efficiency $\eta = 1 - \frac{T_1}{T_2}$, and proved that the efficiency of all reversible cycles has this value. كفاءة دورة

$$\eta = 1 - Q_1/Q_2$$

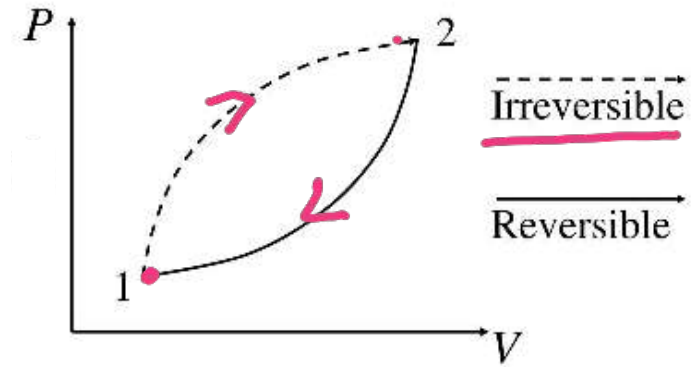
We consider an arbitrary reversible cycle and represent it as a continuous contour in a P-V diagram.

We have: $\oint \frac{dQ}{T} \leq 0$

where the equal sign holds for reversible processes. The precedent equation is sometimes taken as a statement of the second law.

Finally, we consider the change in entropy in an irreversible process. Let 1--2 be an irreversible change and 2--1 be any reversible path connecting the two states in the P- V diagram of Figure . Then the precedent equation becomes:

$$\oint \frac{dQ}{T} = \underbrace{\int_1^2 \frac{dQ}{T}} + \underbrace{\int_2^1 \frac{dQ_r}{T}} \leq \underline{0}$$



Changing the order of integration and the sign of the second term we have:

$$\underbrace{\int_1^2 \frac{dQ}{T}} \leq \int_2^1 \frac{dQ_r}{T} = \underline{S_2 - S_1}$$

Thus: $\underline{\Delta S = S_2 - S_1} \geq \underbrace{\int_1^2 \frac{dQ}{T}}$ Or $\underline{dS \geq \frac{dQ}{T}}$

For an isolated system: $\underline{dQ = 0}$ and $\underline{dS \geq 0}$ Or $\Delta S = S_2 - S_1 \geq 0$

for a finite process. We conclude that:

The entropy of an isolated system increases in any irreversible process and is unaltered in any reversible process.

This is the principle of increasing entropy. It is to be noted that this statement refers to net entropy changes.

Carnot cycle

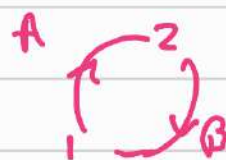
$$\frac{Q_1}{T_1} + \frac{Q_2}{T_2} = 0$$

$$\frac{Q}{T} \Rightarrow \text{Carnot's relation}$$

efficiency (الكفاءة) $\Rightarrow \eta = 1 - \frac{T_c}{T_h}$

Clausius inequality

$$\oint \frac{dQ}{T} \leq 0$$



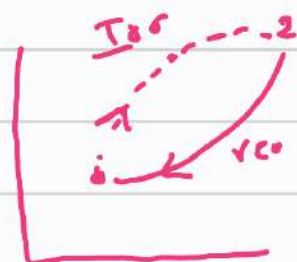
منصبة كل مجموع العملية الحرارية

for reversible process $\Rightarrow \oint \frac{dQ_r}{T} = 0$

for irreversible process $\Rightarrow \oint \frac{dQ}{T} < 0$

$$\oint ds = \oint \frac{dQ}{T}$$

$$\oint \frac{dQ}{T} = \int_1^2 \frac{dQ}{T} + \int_2^1 \frac{dQ_r}{T} \leq 0$$



$|dW_r| \geq |dW|$

$$\int_2^1 \frac{dQ_r}{T} \geq \int_1^2 \frac{dQ}{T}$$

$$\int_2^1 \frac{dQ_r}{T} = S_2 - S_1 = \Delta S$$

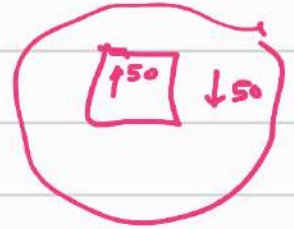
for Isolated system $dQ = 0$:

$$\Delta S = S_2 - S_1$$

موجبه ←
↙ ds

الاستردى لا يرقم صفردل دائماً فزدار لاي كماله
عزلة
الاستردى فو الكون دائماً في تزايد

Reversible



$$\Delta S = 0 = \Delta S_{\text{system}} + \Delta S_{\text{surrounding}}$$

Irreversible

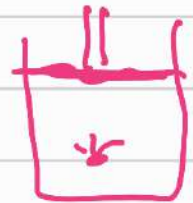
$$\Delta S > 0 \Rightarrow \Delta S_{\text{system}} + \Delta S_{\text{surrounding}} > 0$$

adiabatic process $dQ = 0$

$$\Delta S = 0$$

EXAMPLE 7-1 Entropy Change during an Isothermal Process

A piston-cylinder device contains a liquid-vapor mixture of water at 300 K. During a constant-pressure process, 750 kJ of heat is transferred to the water. As a result, part of the liquid in the cylinder vaporizes. Determine the entropy change of the water during this process.



$$Q = 750 \text{ kJ}$$

$$\Delta S = ??$$

The system undergoes an internally reversible, isothermal process, and thus its entropy change can be determined directly from Eq. 7-6 to be

$$\Delta S_{\text{sys, isothermal}} = \frac{Q}{T_{\text{sys}}} = \frac{750 \text{ kJ}}{300 \text{ K}} = \underline{2.5 \text{ kJ/K}}$$

$$\Delta S = 2.5 \text{ kJ/K}$$

$$\Delta S = \frac{\Delta Q}{T}$$

$$\Delta S = \frac{750}{300}$$

Example:

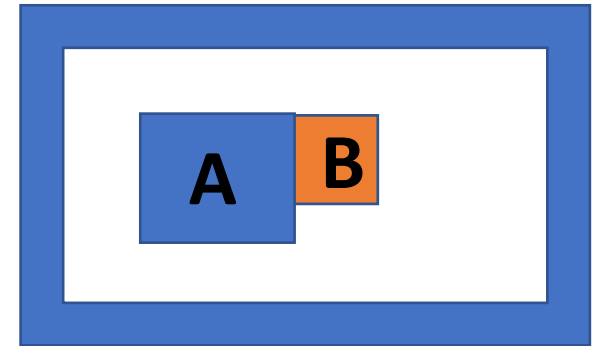
$$dQ=0$$

Consider ~~two~~ ^{two} body in thermal contact in an adiabatic enclosure.

If the heat flows from body A to body B at a lower temperature, with both bodies contained in an adiabatic enclosure, ΔS_A is then negative but: $\Delta S = \Delta S_A + \Delta S_B$ will still be positive

If then, our universe consists of a system and its surroundings, it follows that:

$$\Delta S_{universe} = \Delta S_{system} + \Delta S_{surrounding} \geq 0$$



Enclosure Adiabatic



ABSOLUTE TEMPERATURE

$$\frac{|Q_1|}{|Q_2|} = \frac{T_1}{T_2}$$

The Carnot cycle together with Carnot's theorem can serve as the basis for defining an absolute temperature scale. Carnot's theorem shows that the ratio $|Q_1|/|Q_2|$ has the same value for all reversible engines that operate between the same temperatures. The special fact about a reversible Carnot cycle is that the efficiency is independent of the nature of the working substance. It can therefore be used to define an absolute scale of temperature as follows. لا تعينه على نوع

The definition of the Kelvin scale is completed by assigning to T_1 in Equation: $\frac{|Q_1|}{|Q_2|} = \frac{T_1}{T_2}$ the value of 273.16 K, the temperature of the triple point of water. $T = \frac{|Q_1|}{|Q_2|} T_1$

For a Carnot engine operating between temperatures T and T_1 , we have: $T = 273.16 \frac{|Q_1|}{|Q_2|}$

The smallest value of Q is zero and the corresponding value of T is zero, called absolute zero. In a Carnot cycle, heat is transferred during the isothermal processes. Hence, if a system undergoes a reversible isothermal process without heat transfer, the temperature at which the process takes place is absolute zero. This is a fundamental definition of absolute zero.

absolute Temp
لتعريف

COMBINED FIRST AND SECOND LAWS

We saw early in the chapter that for a reversible process,

$$dU = dQ_r - dW_r = TdS - PdV$$

In its most general form, the first law can be written:

$$dU = dQ - dW \quad (2) \quad (\text{general})$$

The second law states that: $TdS = dQ_r > dQ$ for an irreversible process.

We can write: $dQ_r = dQ + \varepsilon$ (3) $\varepsilon > 0$

(3) In (1) $\rightarrow dU = dQ + \varepsilon - dW_r$ (4)

From (2) and (4) we have: $dW = dW_r - \varepsilon$

We conclude that, the total work done by the system is the reversible configuration work (the useful mechanical work) plus the (negative) dissipative work associated with frictional forces.

$$dU = dQ - dW = dQ_r - \varepsilon - (dW_r - \varepsilon)$$

Or: $dU = TdS - PdV$ (general) (5)

The equation (5) is most important equation in classical thermodynamics

$$dU = dQ_r - dW_r$$

$$du = Tds - PdV$$

(1)

$$du = dQ + \varepsilon - dW_r$$

$$du = dQ_r - \varepsilon - dW$$

$$dU = dQ_r - \varepsilon - (dW_r - \varepsilon)$$

العمل الناتج
من النظام في الحالة

Calculation of the Entropy Changes

ENTROPY CHANGES IN REVERSIBLE PROCESSES

To illustrate the calculation of the entropy change, we first consider reversible processes:

$$dQ_r = dU + Pdv \quad \text{or} \quad \frac{dQ_r}{T} = \frac{dU}{T} + \frac{P}{T}dv = dS$$

We shall examine some special cases.

a) Adiabatic process:

$$dQ_r = 0, dS = 0 \text{ and } S = \text{constant.}$$

A reversible adiabatic process is an isentropic (constant entropy) process. We note in passing that an irreversible adiabatic process is not isentropic.

b) Isothermal process:

$$S_2 - S_1 = \int_1^2 \frac{dQ_r}{T} = \frac{Q_r}{T}$$

c) Isothermal (and isobaric) change of phase:

$$S_2 - S_1 = \frac{l}{T}$$

Here l is the Latent heat of transformation

d) Isochoric process: We assume that $u = u(v, T)$ in general. Since $v = \text{constant}$ in an isochoric process,

$u = u(T)$, as for an ideal gas, $dU = c_v dT$. Thus:

$$S_2 - S_1 = \int_1^2 c_v \frac{dT}{T}$$

If c_v is constant over the temperature range $T_2 - T_1$, we have: $S_2 - S_1 = c_v \ln \frac{T_2}{T_1}$

ENTROPY CHANGES IN REVERSIBLE PROCESSES

e- **Isobaric process**: It is convenient to use the specific enthalpy in an isobaric process.

Since: $h = U + Pv$ and $dQ_r = dU + Pdv \rightarrow dh = dU + Pdv + vdP$

$$dh = dQ_r + vdP \rightarrow dS = \frac{dQ_r}{T} = \frac{dh}{T} - \frac{v}{T} dP$$

In general $h = h(T, P)$, here $P = \text{constant}$ then $h = h(T)$ and $dh = c_p dT$

Then: $\Delta S = S_2 - S_1 = \int_1^2 c_p \frac{dT}{T} = c_p \ln \frac{T_2}{T_1}$ (if c_p is constant)

① Isochoric process $dv=0$

$$dQ = dU = C_v dT \quad \checkmark$$

$$\Delta S = \int dS = \int \frac{dQ}{T} = \int \frac{C_v dT}{T}$$

$$\Delta S = C_v \int_{T_1}^{T_2} \frac{dT}{T} = C_v \ln \frac{T_2}{T_1}$$

$$\Delta S = C_v \ln \frac{T_2}{T_1}$$

② Isobaric process $dp=0$

$$dQ = du + p dv = C_p dT$$

$$\Delta S = \int \frac{dQ}{T} = \int \frac{C_p dT}{T} = C_p \int_{T_1}^{T_2} \frac{dT}{T}$$

$$\Delta S = C_p \ln \frac{T_2}{T_1}$$

③ Isothermal process $dU=0$

$$dQ = p dv$$

$$pV = nRT$$
$$p = \frac{nRT}{V}$$

$$\Delta S = \int \frac{dQ}{T} = \int \frac{p dv}{T} = \int \frac{nRT}{V T} dv = nR \ln \frac{V_2}{V_1}$$

$$\Delta S = nR \ln \frac{V_2}{V_1}$$

④ adiabatic process $dQ = 0$

$$\Delta S = \int \frac{dQ}{T} = 0$$

$$\Delta S = 0$$

⑤ for an Ideal gas

$$\Delta S = C_2 \ln \frac{T_2}{T_1} + R \ln \frac{V_2}{V_1}$$

ENTROPY CHANGE OF THE SURROUNDINGS FOR A REVERSIBLE PROCESS

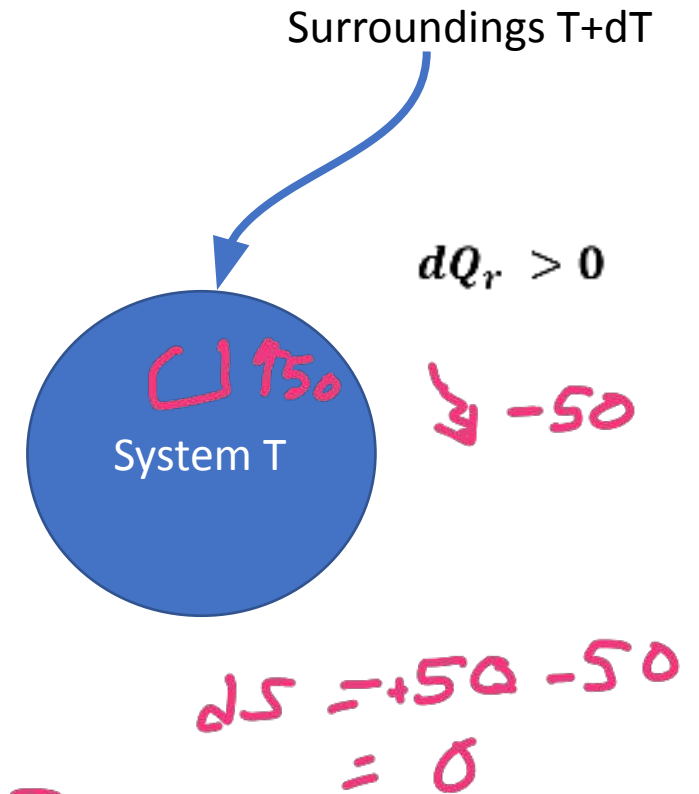
The heat flow into a system from its surroundings in reversible process is shown in the figure

Thus: $dS_{\text{system}} + dS_{\text{surroundings}} = dS_{\text{universe}}$

As: $|dS_{\text{system}}| = -|dS_{\text{surrounding}}|$ and $dS_{\text{universe}} = 0$

In any reversible process, the entropy change of the **universe is always zero**. This means that any change in entropy of the system will be accompanied by an entropy change in the surroundings equal in magnitude but opposite in sign.

Entropy is conserved in a reversible process. Of course, only idealized -processes are reversible; **all natural processes are irreversible**, and entropy is not conserved in general.



جميع العمليات الطبيعية هي عمليات عكسية (الاستدراك غير ممكنة).

ENTROPY CHANGE FOR AN IDEAL GAS

With: $dU = c_v dT$ and $\frac{dQ_r}{T} = \frac{dU}{T} + \frac{P}{T} dv = dS$

Then: $\frac{dQ_r}{T} = \frac{c_v dT}{T} + \frac{P}{T} dv = dS$

for a reversible process. For an ideal gas: $\frac{P}{T} = \frac{R}{v}$

So: $dS = \frac{c_v dT}{T} + \frac{R}{v} dv$

If c_v is constant, we have:

$$\Delta S = S_2 - S_1 = c_v \ln \frac{T_2}{T_1} + R \ln \frac{v_2}{v_1}$$

$$ds = \frac{dQ}{T}$$

$$dQ = ds T$$

$$dU = T ds - P dv$$

$$dU = T ds - \frac{nRT}{v} dv$$

$$\frac{T ds}{T} = \frac{dU}{T} + \frac{nRT}{T v} dv$$

$$ds = \frac{dU}{T} + \frac{R}{v} dv \Rightarrow \int_{s_1}^{s_2} ds = \int_{T_1}^{T_2} \frac{c_v dT}{T} + \int_{v_1}^{v_2} \frac{R}{v} dv = s_2 - s_1 = c_v \ln \frac{T_2}{T_1} + R \ln \frac{v_2}{v_1}$$
$$= s_2 - s_1 = c_p \ln \frac{T_2}{T_1} + R \ln \frac{v_2}{v_1}$$

$$PV = nRT \checkmark$$

$$dU = dQ + P dv$$

$$P = \frac{nRT}{v}$$

ENTROPY CHANGE IN IRREVERSIBLE PROCESSES

How do we calculate the entropy change for an irreversible process when the entropy is only defined in terms of reversible heat flow?

We resort again to an earlier argument. The entropy is a state variable, and the entropy difference is the same between any two equilibrium states regardless of the nature of the process.

Thus, we can find ΔS as for an irreversible process by choosing any convenient reversible path from the initial to the final state and be certain that it is equal to the change produced by the actual irreversible path.

EXAMPLE $\Delta S = S_2 - S_1$ ΔS مثل ΔU لا تعتمد على المسار، بل على الحالة الابتدائية والنهائية



Suppose that 0.5 kg of water at 90°C is cooled to 20°C, the temperature of the surrounding room. The specific heat capacity at constant pressure of water is 4180 J K⁻¹ g⁻¹. The change in entropy of the system (the water) is the change that would occur if the water were cooled reversibly from:

$T_1 = 363 \text{ K}$ and $T_2 = 293 \text{ K}$. 26

Calculate the change in entropy of the system (water), the change in entropy of the surrounding and the change in entropy of the universe. ΔS

$$T_1 = 363 \text{ K} \quad T_2 = 293 \text{ K} \quad c_p = 4180$$

$$m = 0.5 \text{ kg}$$

$$\Delta S = m c_p \ln \frac{T_2}{T_1}$$

$$\Delta S_{\text{water}} = 0.5 (4184) \ln \left(\frac{293}{363} \right) \\ = -448 \text{ J/K}$$

$$\Delta S_{\text{universe}} = 0$$

$$0 = \Delta S_{\text{water}} + \Delta S_{\text{surr}} \\ \Delta S_{\text{sur}} = 448 \text{ J/K}$$

Free expansion of an Ideal gas

$$\Delta S = R \ln \left(\frac{V_2}{V_1} \right) + c_v \ln \left(\frac{T_2}{T_1} \right)$$

Isothermal $\Delta T = 0$

$$\Delta S = R \ln \left(\frac{V_2}{V_1} \right)$$

$$W_r = Q_r$$

$$\Delta Q = T \Delta S$$

$$W = R T_0 \ln \frac{V_2}{V_1}$$

In Free expansion no work done, reversible isothermal
 $W = \Delta S T$

FREE EXPANSION OF AN IDEAL GAS

in the free expansion of an ideal gas, $du = 0$ and $dQ = 0$ so that $dW = 0$ also.

Referring to the figure, we observe that the equations describing the equilibrium end states are:

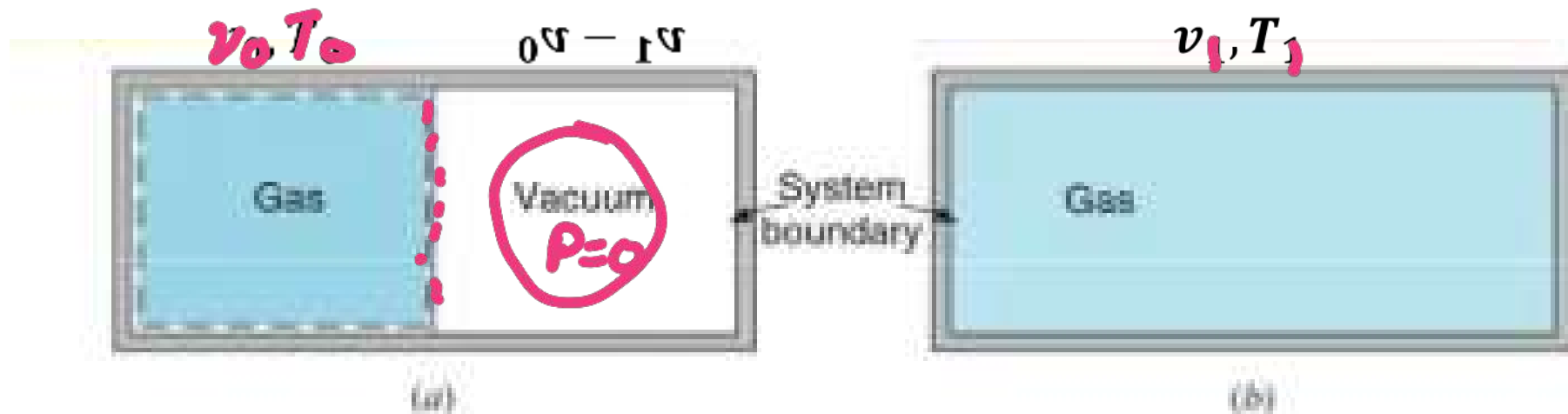
$$\begin{aligned} P_1 V_1 &= n R T_1 \\ P_2 V_2 &= n R T_2 \end{aligned}$$

$$P_0 = \frac{RT_0}{v_0}; \text{ and } P_1 = \frac{RT_1}{v_1}$$

A reversible isothermal process would be described by the equation $Pv = \text{constant}$ or $P_0 v_0 = P_1 v_1$. However, the latter equation does not describe the free expansion because P_1 is initially zero and the process is irreversible.

$$Pv = P_1 v_1$$

X



FREE EXPANSION OF AN IDEAL GAS

$$pv = nRT$$

Nonetheless, the entropy change can be calculated by assuming that a reversible, isothermal expansion takes place between the initial and final states of the system. Thus,

$$dS = c_v \frac{dT}{T} + R \frac{dv}{v} \quad \checkmark \quad (\text{isothermal} \rightarrow dT = 0)$$

$$\begin{aligned} dU &= dQ - p dv \\ dU &= T ds - p dv \\ \frac{dU}{T} &= ds - \frac{p}{T} dv \end{aligned}$$

So: $(\Delta S)_{\text{system}} = S_2 - S_1 = \int_1^2 R \frac{dv}{v} = R \ln \left(\frac{v_2}{v_1} \right)$

$(\Delta S)_{\text{surrounding}} = -(\Delta S)_{\text{system}} > 0$; the system is isolated (adiabatically insulated).

In an irreversible free expansion, the available energy levels become more closely spaced leading to greater randomness and increased entropy.

For a reversible isothermal expansion, the work done would be:

$$W_r = \underline{RT_0} \ln \left(\frac{v_2}{v_1} \right)$$

Since: $dU = 0$; $Q_r = W_r$ so that: $\Delta S = \frac{Q_r}{T} = R \ln \left(\frac{v_2}{v_1} \right)$

$$\begin{aligned} ds &= \frac{c_v dT}{T} + \frac{R dv}{v} \\ \Delta S &= c_v \ln \frac{T_2}{T_1} + R \ln \frac{v_2}{v_1} \end{aligned}$$

In a free expansion no work is done but the change in entropy in the irreversible process is as if work were done in a reversible, isothermal process between the same end points.

The Tds Equations

$$du = dQ - Pdv$$
$$\underline{Tds} = du + Pdv$$

From the combined first and second laws expressed as:

$$TdS = dU + P dv$$

We can obtain some powerful results known as the "TdS equation".

They involve writing the specific entropy as function of two independent coordinates, that is, two of the three fundamental state variable P, T and v. the equations are:

$$TdS = c_v dT + T \left(\frac{\partial P}{\partial T} \right)_v dv = c_v dT + \frac{T\beta}{K} dv; \quad S = S(T, v)$$

متغيرين متعلقين T و v
متغير تابع P

$$T dS = c_p dT - T \left(\frac{\partial v}{\partial T} \right)_P dP = c_p dT - T\alpha \beta dP; \quad S = S(T, P)$$

متغيرين متعلقين T و P
متغير تابع v

$$T dS = c_p \left(\frac{\partial T}{\partial v} \right)_P dv + c_v \left(\frac{\partial T}{\partial P} \right)_v dP = \frac{c_p}{\beta v} dv + \frac{c_v K}{\beta} dP; \quad S = S(P, v)$$

متغيرين متعلقين P و v
متغير تابع T

کتابچه معادله Tds با متغیرهای مستقل و متغیر تابع

The Tds Equations

$$\underline{ds} = \frac{dQ_r}{T}$$

The Tds equations have a variety of uses:

- 1) they give the heat transferred in a reversible process $dQ_r = TdS$.
- 2) the entropy can be obtained by dividing by T and integrating.
- 3) the equations express the heat flow or entropy in terms of measurable properties such as: c_p , β , K , T , ect ...
- 4) they can be used to determine the difference in the specific heat capacities c_p and c_v
- 5) the equations can provide relations between pairs of coordinates in a reversible adiabatic process in which $ds = 0$.

$$du = \underline{c_v} dT$$

$$du = \underline{c_p} dT$$

$$dU = dQ - PdV$$

$$dQ = du + PdV$$

$$ds = \frac{du}{T} + \frac{PdV}{T}$$

ENTROPY CHANGE FOR A LIQUID OR SOLID

The equation of state of a liquid or solid is, to a first approximation

$$v = v_0 [1 + \beta(T - T_0) - k(P - P_0)]$$

The second TdS equation: $T dS = c_p dT - T \left(\frac{\partial v}{\partial T} \right)_P dP$ المعادلة الثانية صفا معادلات $T dS$

Setting: $\left(\frac{\partial v}{\partial T} \right)_P = \beta v_0$

We obtain:

$$\int dS = \int c_p \frac{dT}{T} - \int \beta v_0 dP$$

Integrating we have: $\Delta S = S_2 - S_1 = c_p \ln \left(\frac{T}{T_0} \right) - \beta v_0 (P - P_0)$

The entropy increases if the temperature increases and decreases if the pressure increases.

تزداد S إذا زادت درجة الحرارة وتقل عندما يزداد الضغط

التغير في S
في حالة لا صلب
الماء والسائل

Tds equation

$$Tds = du + pdv$$

① باقة العاقلين $S(T, v)$

$$Tds = c_v dT + T \left(\frac{\partial p}{\partial T} \right)_v dv \quad \beta = \frac{1}{\gamma} \frac{\partial p}{\partial T}$$

$$Tds = c_v dT + T \frac{\beta}{\gamma} dv$$

② باقة العاقلين $S(T, p)$

$$Tds = c_p dT - T \left(\frac{\partial v}{\partial T} \right)_p dp$$

$$Tds = c_p dT - T \gamma \beta dp \quad \frac{\partial v}{\partial T} = \gamma \beta$$

③ باقة العاقلين $S(p, v)$

$$Tds = c_p \left(\frac{\partial T}{\partial v} \right)_p dv + c_v \left(\frac{\partial T}{\partial p} \right)_v dp$$

$$= \frac{c_p}{\gamma \beta} dv + \frac{c_v \gamma}{\beta} dp$$